This listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

- 1. (Currently Amended) A process for sequestrating carbon in the atmosphere, comprising:
 - a) a step for concentrating CO₂ in the <u>a</u> liquid phase, said step comprising any of the following: (i) liquefying CO₂ in the <u>a</u> liquid phase under pressure up to the supercritical state; (ii) absorbing CO₂ in a polar aprotic liquid, not miscible with water, or miscible with water in various proportions; (iii) absorbing CO₂ in an aqueous phase containing an alcohol and/or an amine; (iv) absorbing CO₂ in the hydrated form in a solvent, activated by an enzymatic pathway, with the provision that in (iii) and (iv) resultant absorbed CO₂ in the an aqueous phase is transferred to a water-insoluble ionic liquid medium;
 - a step for electro-reduction of resultant <u>pressurized CO₂ from step (i)</u> liquid phase eontaining liquid or <u>resultant</u> absorbed CO₂, in an <u>said</u> aprotic medium <u>from step (ii)</u> or resultant CO₂ from step (iii) or step (iv) transferred to a water-insoluble ionic medium to oxalic acid or formic acid in which the carbon changes to oxidation number +3;
 - c) if appropriate, a step for extracting said oxalic acid or formic acid in an aqueous phase; and
 - a step for mineralization by reacting said oxalic acid or formic acid with a carbonate of an element M, producing a mineral in which the atomic ratio C/M is about 2/1, wherein M is any metallic element with an oxidation number of +2, and C is carbon, and wherein the oxalic acid and formic acid are in an acid or salt form.

- 2. (Currently Amended) A process according to claim 1, characterized in that step a) for concentration in the liquid phase comprises the liquefying of said CO₂, the liquid CO₂ then being obtained under the said pressure, up to the supercritical state.
- 3. (Currently Amended) A process according to claim 1, characterized in that step a) for concentration in the liquid phase comprises the absorbing of the CO₂ in a the polar aprotic liquid, not miscible with the water or miscible with the water in various proportions.
- 4. (Currently Amended) A process according to claim 1, characterized in that step a) for concentration concentrating CO₂ in the liquid phase comprises said absorbing of CO₂ in an aprotic ionic liquid not miscible with water or miscible with water in various proportions.
- 5. (Previously Presented) A process according to claim 4, characterized in that said ionic liquid comprises 1-butyl-3-methylimidazolium hexafluorophosphate.
- 6. (Currently Amended) A process according to claim 1, characterized in that step a) for concentration in the liquid phase comprises the absorbing of the CO₂ in an the aqueous phase containing an the alcohol and/or an the amine.
- 7. (Currently Amended) A process according to claim 1, characterized in that step a) for concentration in the liquid phase comprises the absorbing of the CO₂ in a the hydrated form being activated by an the enzymatic pathway.
- 8. (Previously Presented) A process according to claim 7, characterized in that the hydration activating enzyme comprises carbonic anhydrase.
- 9. (Previously Presented) A process according to claim 8, characterized in that the resultant liquid phase obtained is then recycled to a process for absorption of CO₂ in an aqueous phase in the presence of an alcohol and/or amine.

- 10. (Previously Presented) A process according claim 9, characterized in that the aqueous phase obtained is recycled to a liquefaction process of CO₂ under pressure.
- 11. (Currently Amended) A process according to claim 6, characterized in that the <u>resultant</u> aqueous solution obtained is transferred by a liquid-liquid extraction process to an ionic liquid medium which is insoluble in water.
- 12. (Previously Presented) A process according to claim 1, in which the electro-reduction step b) is carried out at a pH in the range of 3 to 10 and with an anode maintained at a potential of +0.5 to -3.5 volts with respect to a normal hydrogen electrode.
- 13. (Previously Presented) A process according to claim 12, in which the pH is in the range of 3 to 7.
- 14. (Previously Presented) A process according to claim 12, in which the anode used in the electro-reduction step is constituted by platinum, diamond-doped with boron or carbon doped with nitrogen.
- 15. (Previously Presented) A process according to claim 1, in which the electro-reduction step b) is carried out in liquid CO₂ under pressure.
- 16. (Previously Presented) A process according to claim 1, in which a compound from electroreduction step b) comprises said oxalic acid or an oxalate.
- 17. (Previously Presented) A process according to claim 16, in which the oxalic acid or oxalate, obtained in the aprotic medium, is re-extracted by an aqueous phase.
- 18. (Previously Presented) A process according to claim 1 in which, at the end of step a), liquid CO₂ is injected into a subterranean CO₂ store.

- 19. (Previously Presented) A process according to claim 18, in which electro-reduction step b) is carried out in the subterranean CO₂ store.
- 20. (Previously Presented) A process according to claim 1, incorporating step (c) in which a final mineralization step comprises an attack of a carbonated mineral by an aqueous solution of oxalic acid or formic acid from the extracting step (c).
- 21. (Previously Presented) A process according to claim 19, in which said mineral comprises a calciferous or magnesia-containing carbonated mineral.
- 22. (Previously Presented) A process according to claim 1, in which the element M is calcium and the mineral produced is Whewellite, CaC₂O₄.H₂O.
- 23. (Previously Presented) A process according to claim 1, in which the mineralization step comprises bringing an aqueous solution of oxalic acid or formic acid derived from the extracting step into contact with a calciferous or magnesia-containing sedimentary rock.
- 24. (Previously Presented) A process according to claim 1, in which a final mineralization step comprises injection into a substratum.
- 25. (Previously Presented) A process according to claim 2, in which the electro-reduction step b) is carried out in liquid CO₂ under pressure.
- 26. (Previously Presented) A process according to claim 25, incorporating step (c) in which a final mineralization step comprises an attack of a carbonated mineral by an aqueous solution of oxalic acid or formic acid derived from the extraction step (c).
- 27. (Previously Presented) A process according to claim 26, in which said carbonated mineral comprises a calciferous or magnesia-containing carbonated mineral.

28-29. (Cancelled)